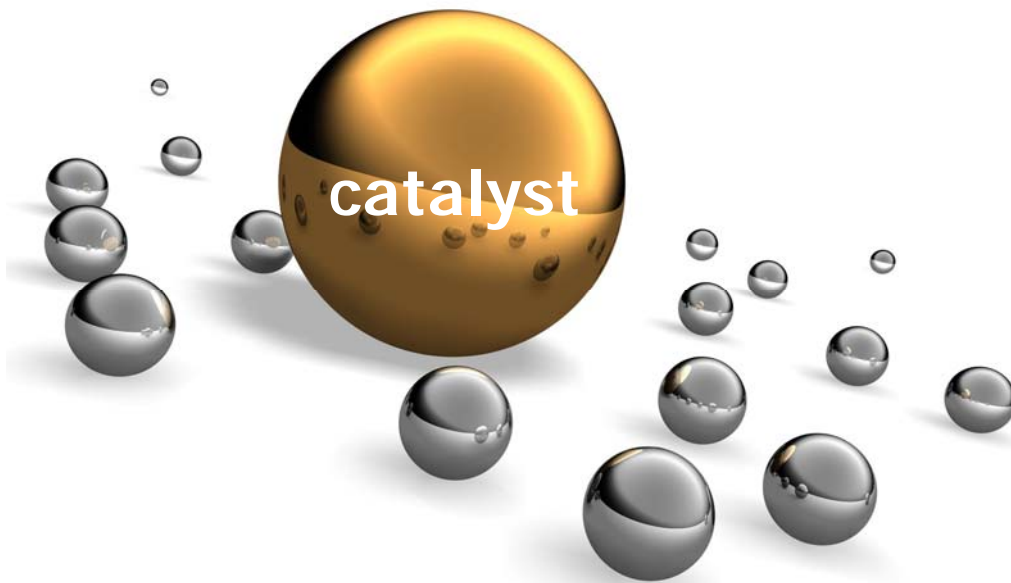
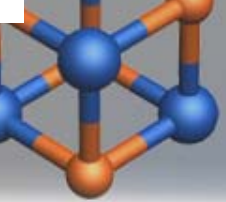


Metallkatalysatoren für Depolymerisationsprozesse



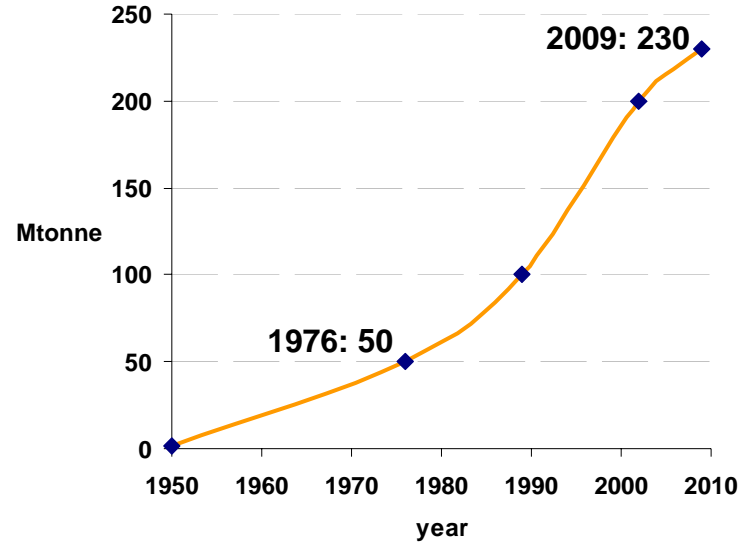
Stephan Enthaler



Introduction

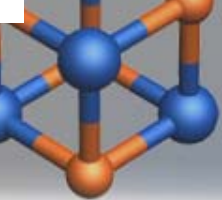


World plastics production



“Any future scenario where plastics do not play an increasingly important role in human life therefore seems unrealistic.”

A. L. Andrady, M. A. Neal, *Phil. Trans. R. Soc. B* **2009**, 364, 1977.



Introduction

Backside of the success (I):

- Plastics derived mainly from petrochemicals
- 4% of the annual petroleum production
- Additional 3-4% for manufacture energy



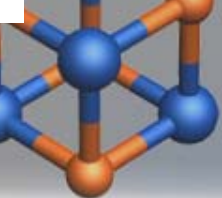
Backside of the success (II):

- plastic production: **55 Mtonnes** (2007, EU)

vs.

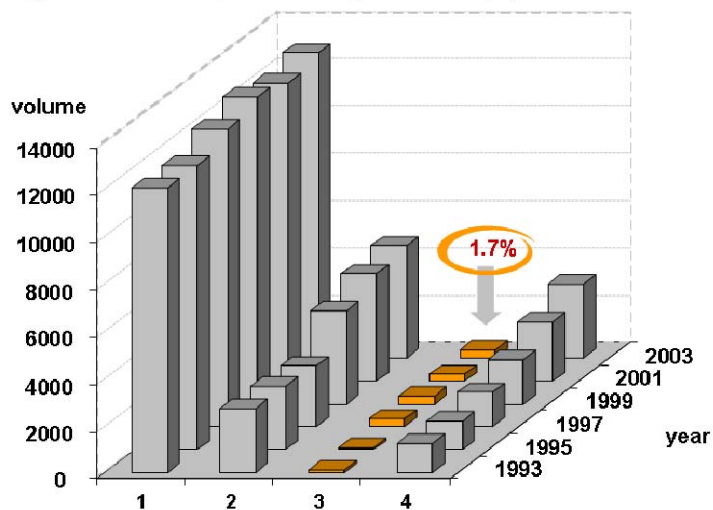
- end-of-life-plastics: **25 Mtonnes** (2007, EU)





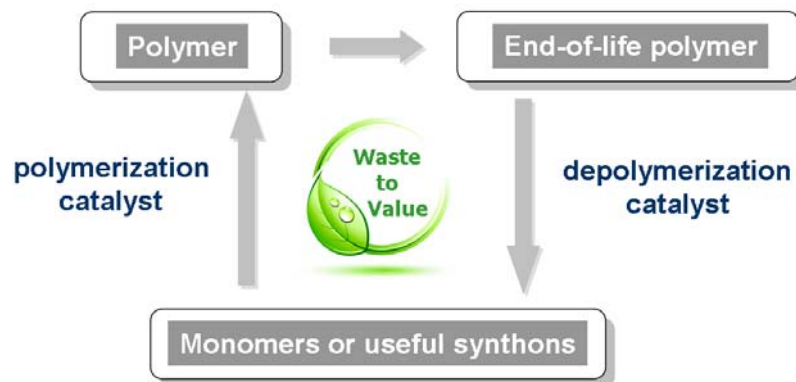
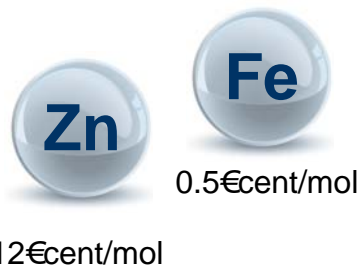
Introduction

Figure 2. Volumes of plastic waste (Western Europe)



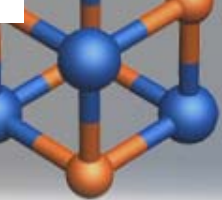
- 1: landfill
- 2: energy recovery (thermal recycling)
- 3: feedstock recycling
- 4: mechanical recycling (downcycling)

Ru: 150€/mol
Rh: 2484€/mol
Pd: 1460 €/mol



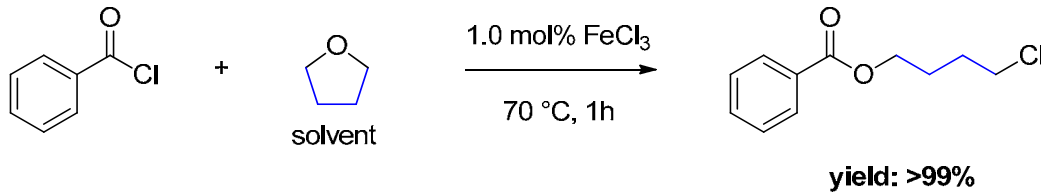
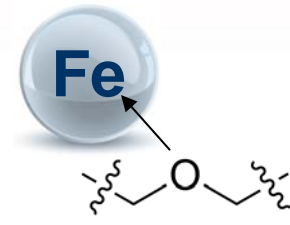
Depolymerization requirements

- abundant and cheap catalyst/reagents
- robust
- low toxicity
- non-inert conditions
- low-temperature
- solvent-free

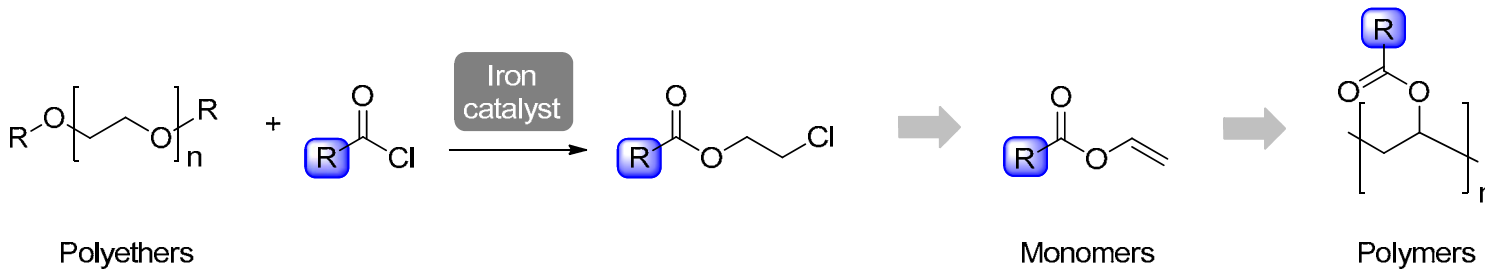


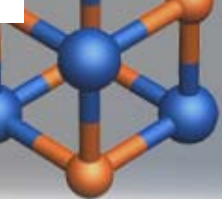
Depolymerization of Polyethers

Polyether: Polyethylene glycol (24.000.000 t/a)
 Polypropylene oxide (6.600.000 t/a)
 Polytetrahydrofuran (250.000 t/a)

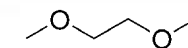
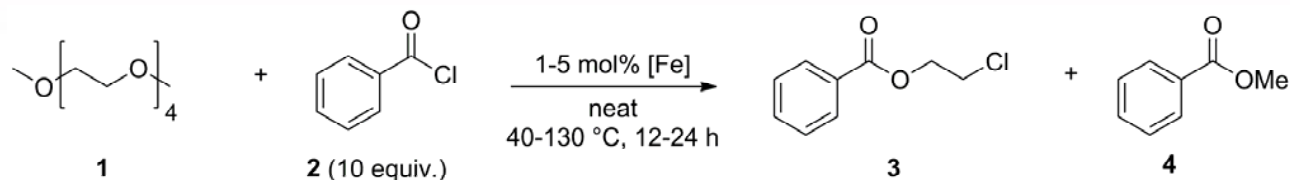


Transfer of the concept



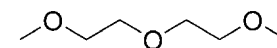


Depolymerization of Polyethers

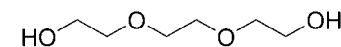


Yield: 79%

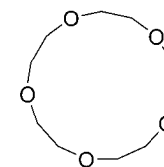
Entry ^[a]	Iron source (mol%)	T [°C]	Yield (3) [%] ^[b]
1	--	130	<1
2	FeCl ₂ •4H ₂ O (5)	130	87
3	FeCl ₃ (5)	130	81
4	FeBr ₃ (5)	130	69
5	Fe(ClO ₄) ₂ •H ₂ O (5)	130	71
6	Fe(ClO ₄) ₃ •4H ₂ O (5)	130	73
7	FeCl ₂ •4H ₂ O (2.5)	130	82
8	FeCl ₂ •4H ₂ O (1.0)	130	68
9	FeCl ₂ •4H ₂ O (5)	100	86
10	FeCl ₂ •4H ₂ O (5)	80	69



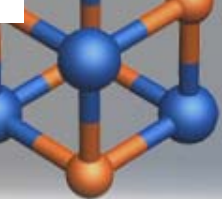
Yield: 81%



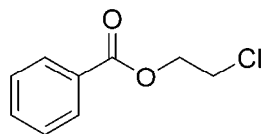
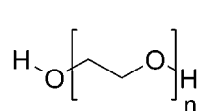
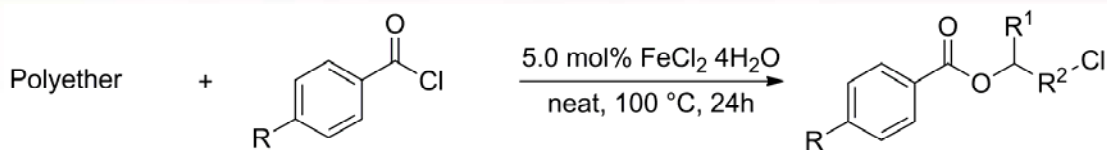
Yield: 73%



Yield: 82%

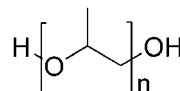


Depolymerization of Polyethers



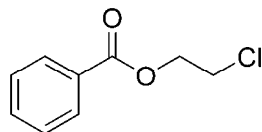
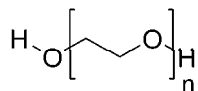
Polyethylene glycol
($M_n \sim 100.000 \text{ g/mol}$)

Yield: 89%



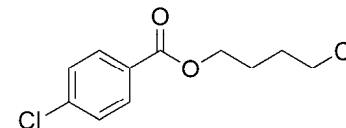
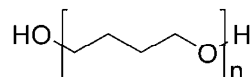
Polypropylene oxide
($M_n \sim 2500 \text{ g/mol}$)

Yield: 68%



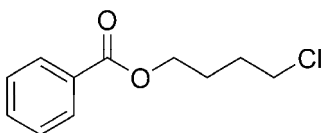
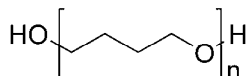
Polyethylene glycol
($M_n \sim 1.000.000 \text{ g/mol}$)

Yield: 95%



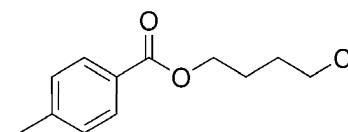
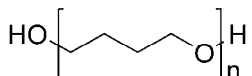
Polytetrahydrofuran
($M_n \sim 1000 \text{ g/mol}$)

Yield: 92%



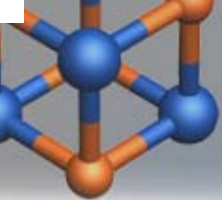
Polytetrahydrofuran
($M_n \sim 1000 \text{ g/mol}$)

Yield: 83%

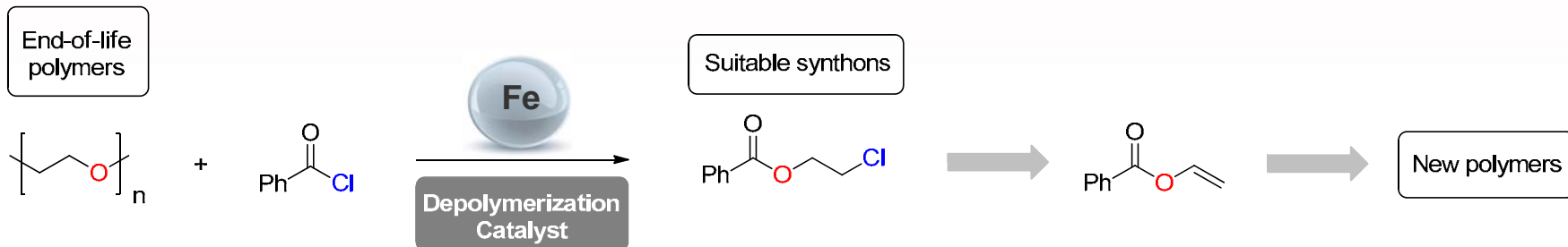


Polytetrahydrofuran
($M_n \sim 1000 \text{ g/mol}$)

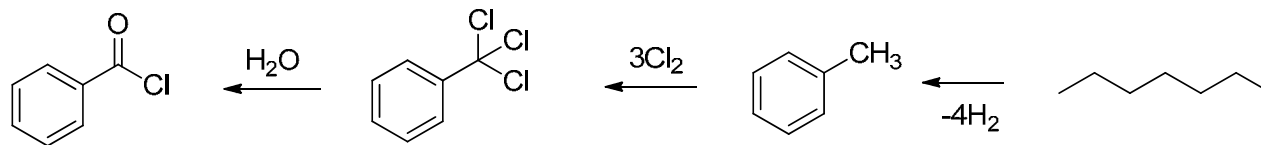
Yield: 89%



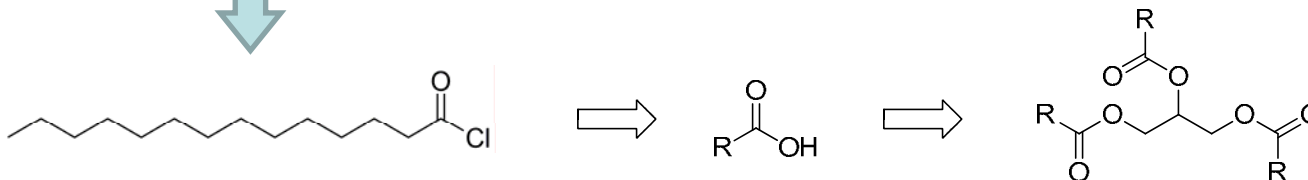
Depolymerization of Polyethers



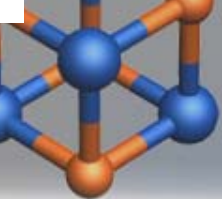
Problem:



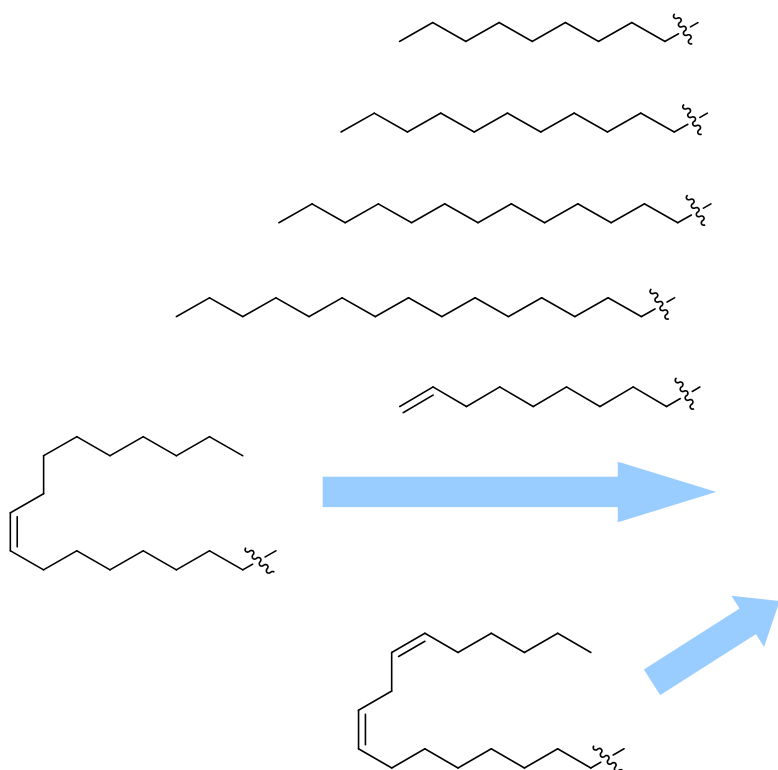
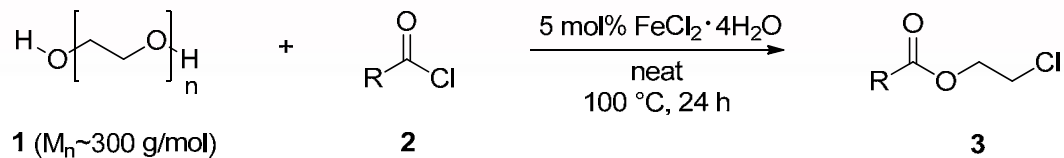
Option:



Renewable resources
 ■ fatty acid chlorides

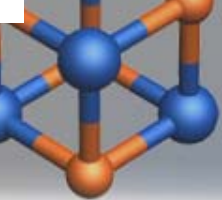


Depolymerization of Polyethers

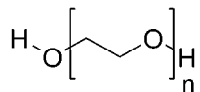
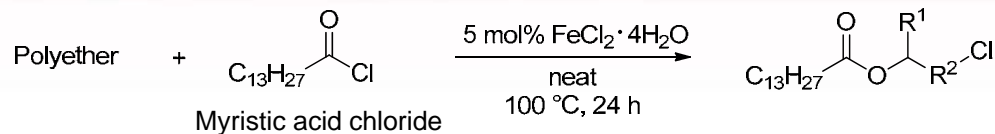


Entry	Substrate (C:D) ^[a]	Yield (3) [%]
1	capric acid chloride (10:0)	78
2	lauroyl chloride (12:0)	77
3	myristoyl chloride (14:0)	82
4	palmitoyl chloride (16:0)	75
5	10-undecenoyl chloride (11:1)	<1
6	oleic acid chloride (18:1)	39
7	linoleic acid chloride (18:2)	<1

[a] C:D = number of carbons: number of double bonds.

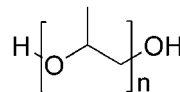


Depolymerization of Polyethers



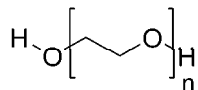
Yield: 69%

Polyethylene glycol
($M_n \sim 1.000 \text{ g/mol}$)



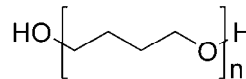
Yield: 77%

Polypropylene oxide
($M_n \sim 2500 \text{ g/mol}$)



Yield: 56%

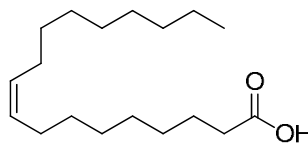
Polyethylene glycol
($M_n \sim 1.000.000 \text{ g/mol}$)



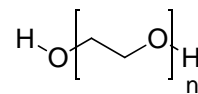
Yield: 57%

Polytetrahydrofuran
($M_n \sim 1000 \text{ g/mol}$)

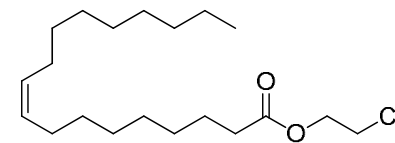
▪ ***in situ* generation of the acid chloride**



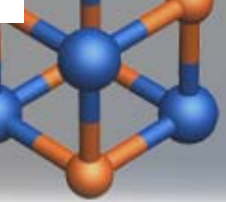
a) SOCl_2 , 80°C , 2 h
 b) 5 mol% $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$,
 100°C , 24 h



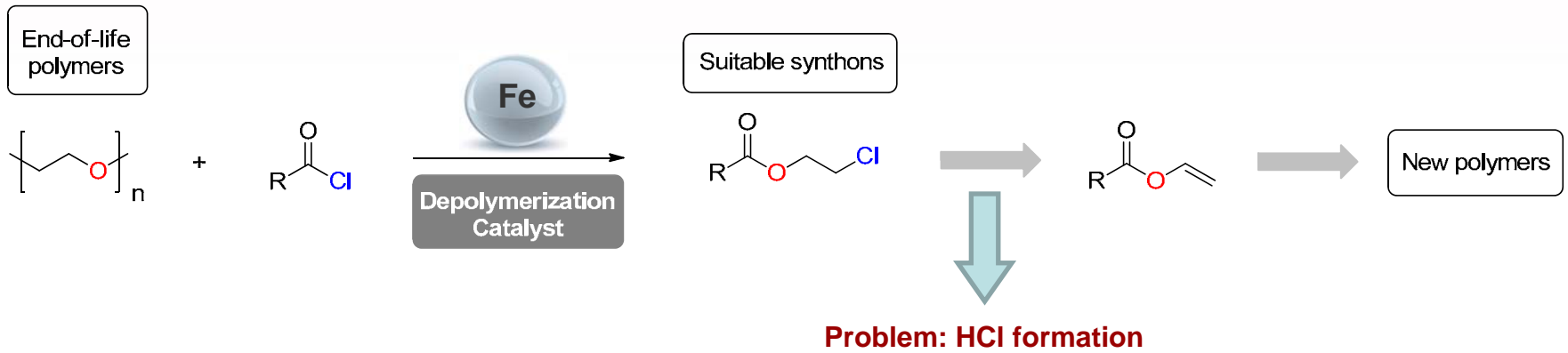
1 ($M_n \sim 300 \text{ g/mol}$)



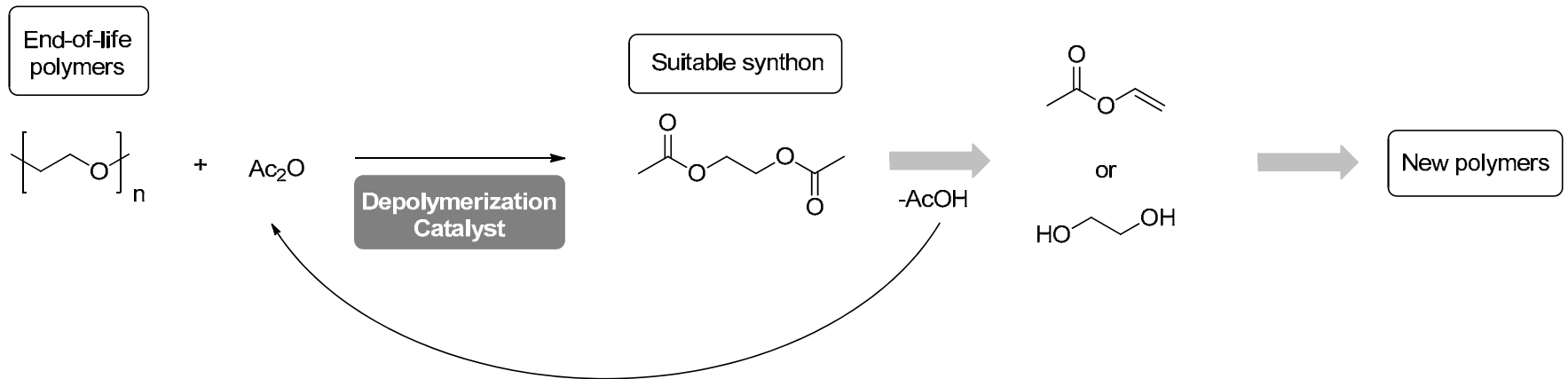
yield: 35%

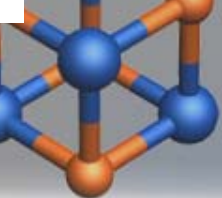


Depolymerization of Polyethers

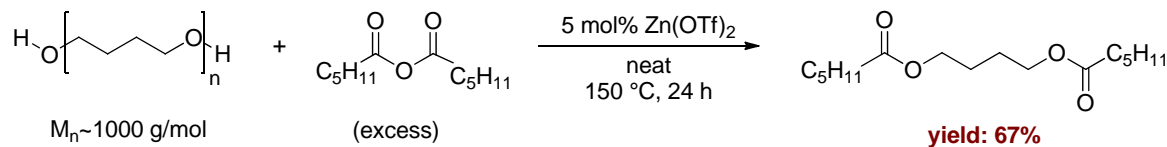
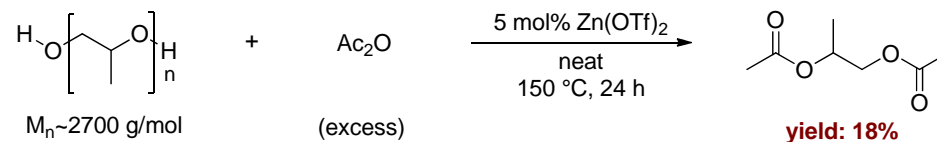
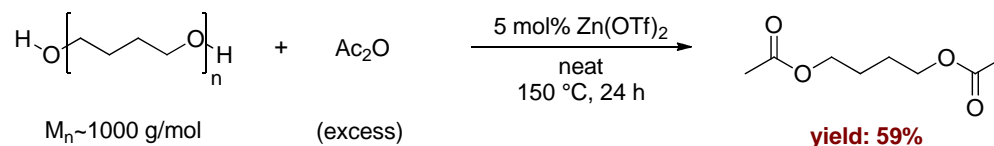
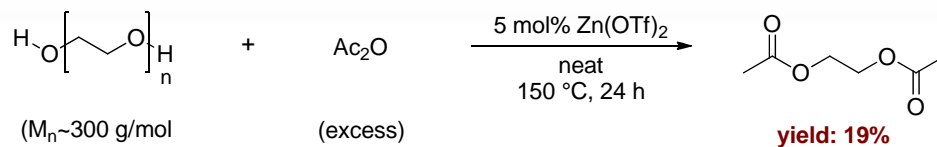


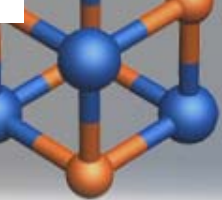
Option:



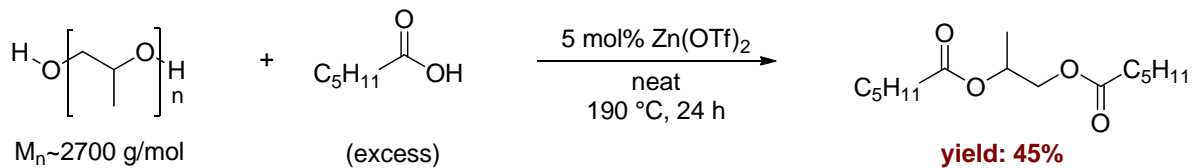
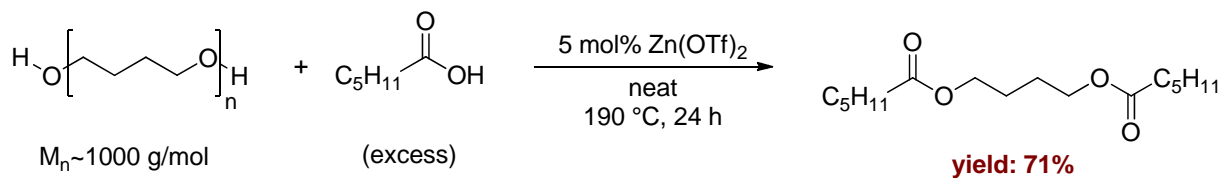
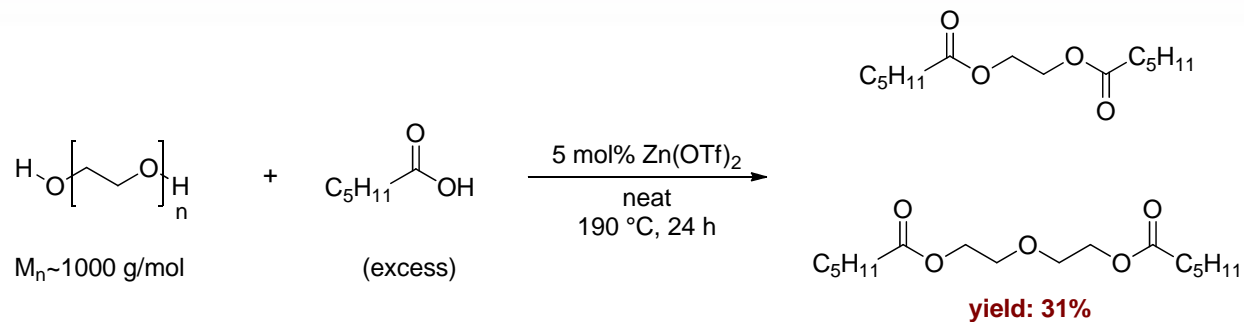


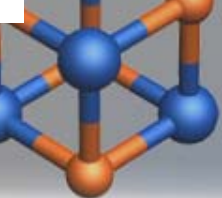
Depolymerization of Polyethers



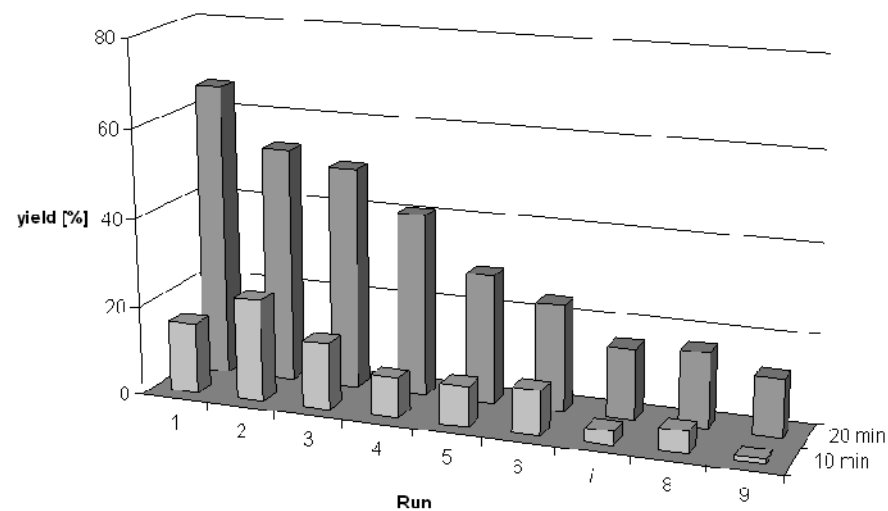
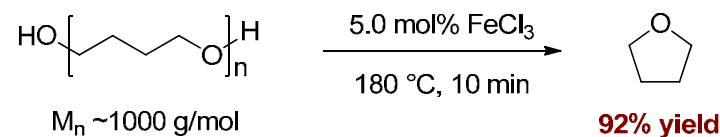
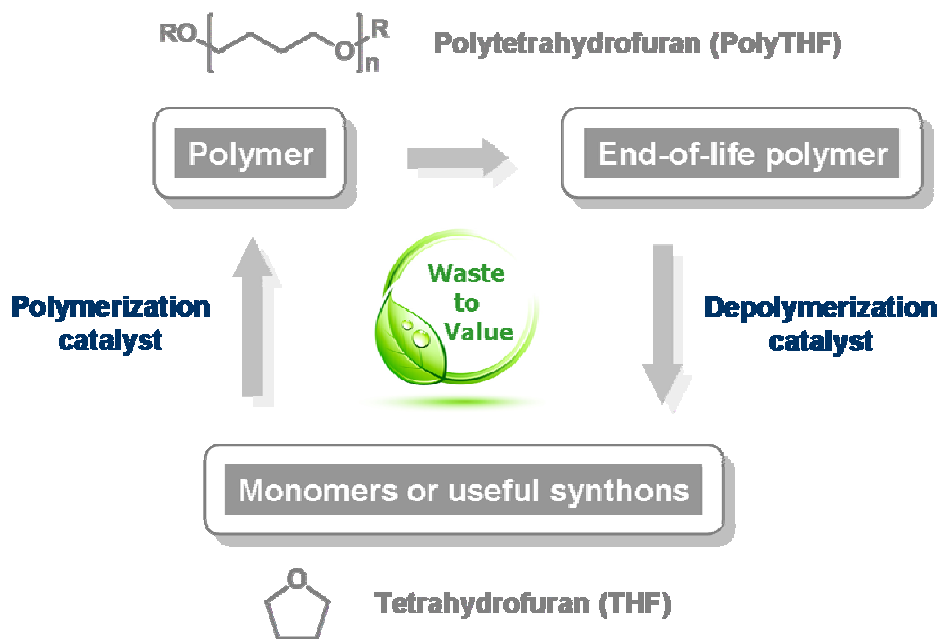


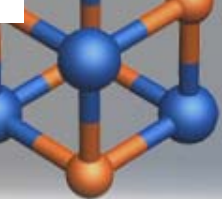
Depolymerization of Polyethers



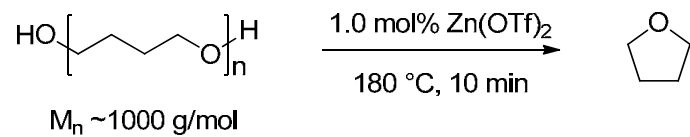
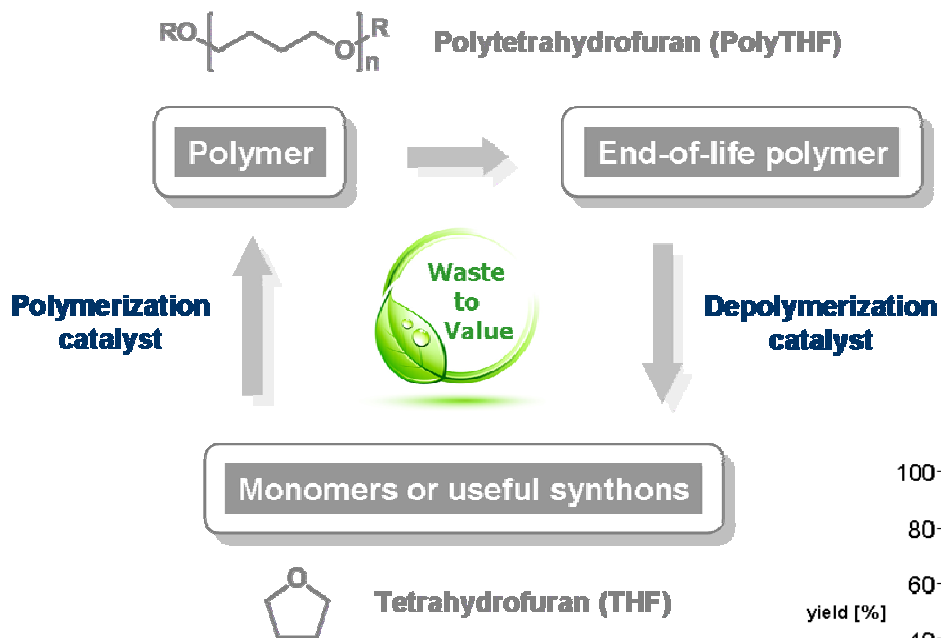


Depolymerization of Polyethers

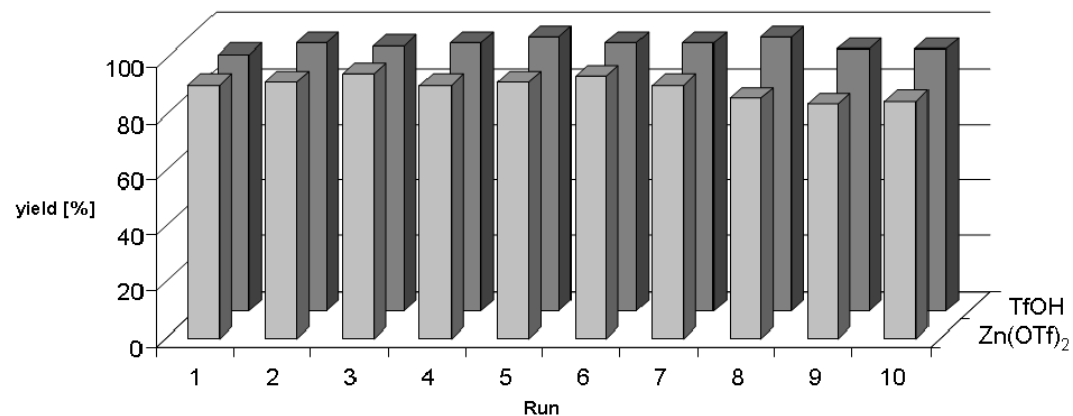


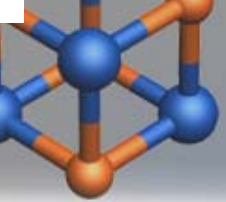


Depolymerization of Polyethers



TON = 900
TOF = 180 h⁻¹

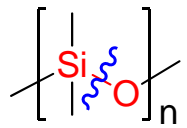




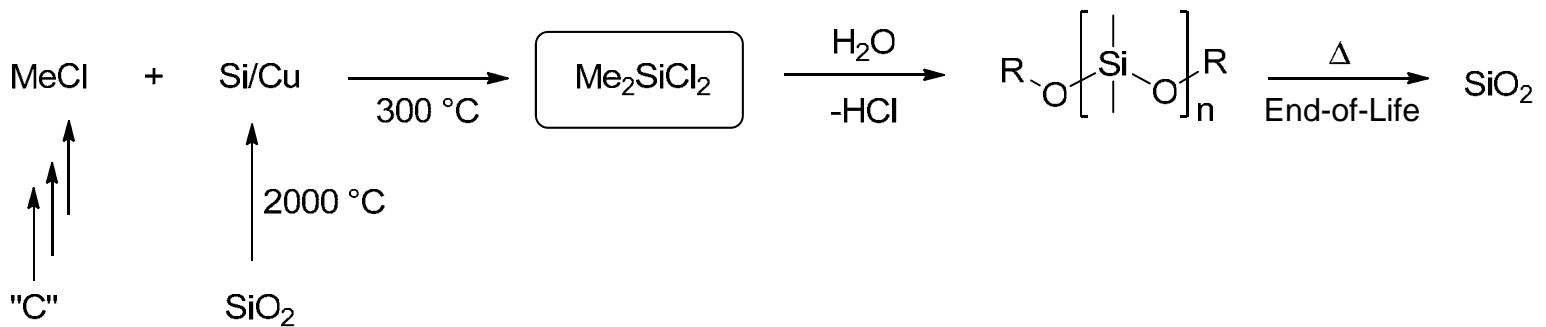
Depolymerization of Silicones

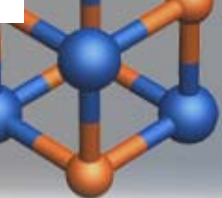


Transfer of the concept to polysiloxanes?

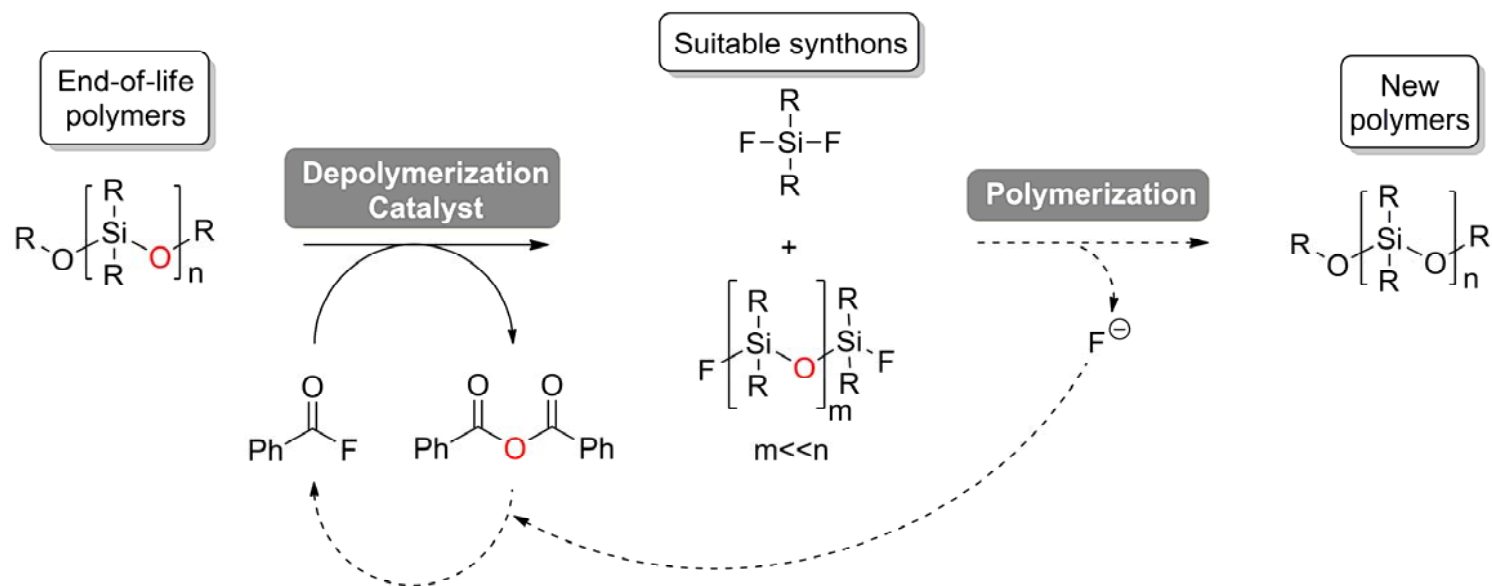


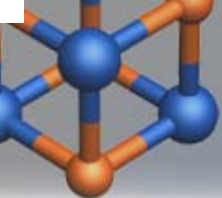
▪ Polysiloxane synthesis



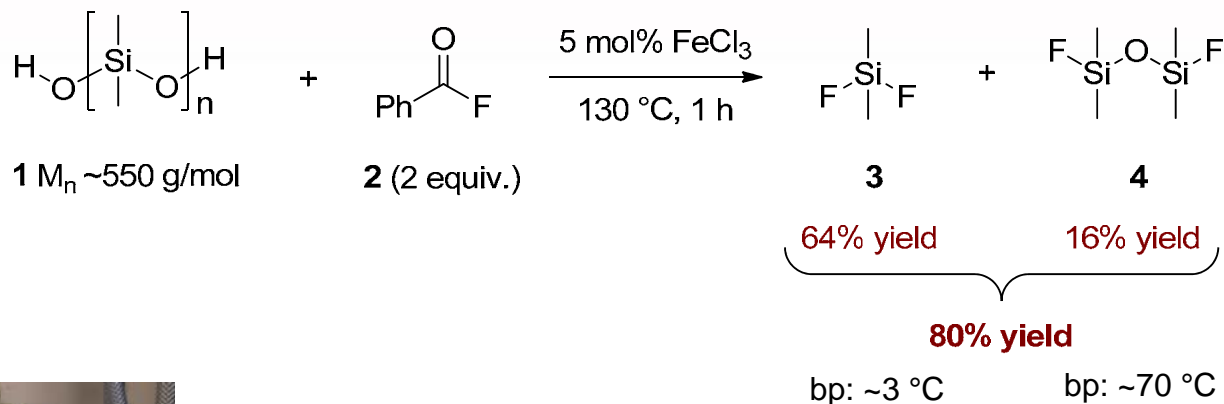


Depolymerization of Silicones

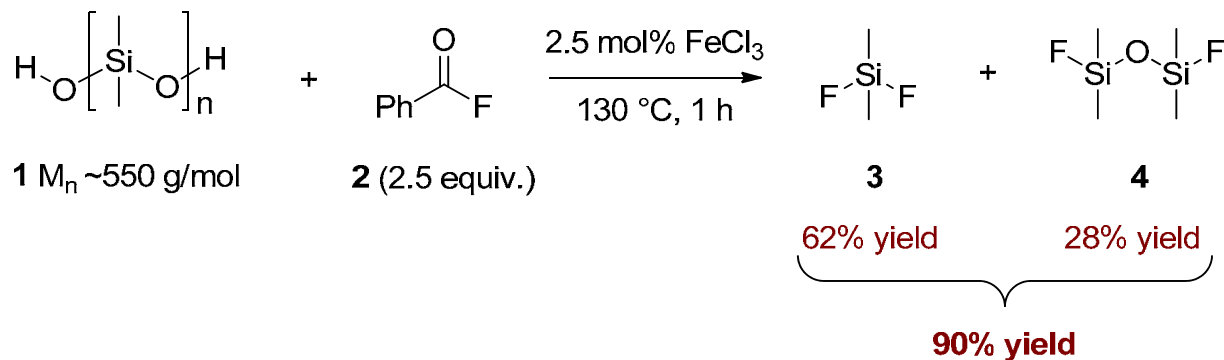


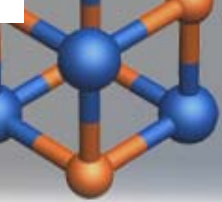


Depolymerization of Silicones

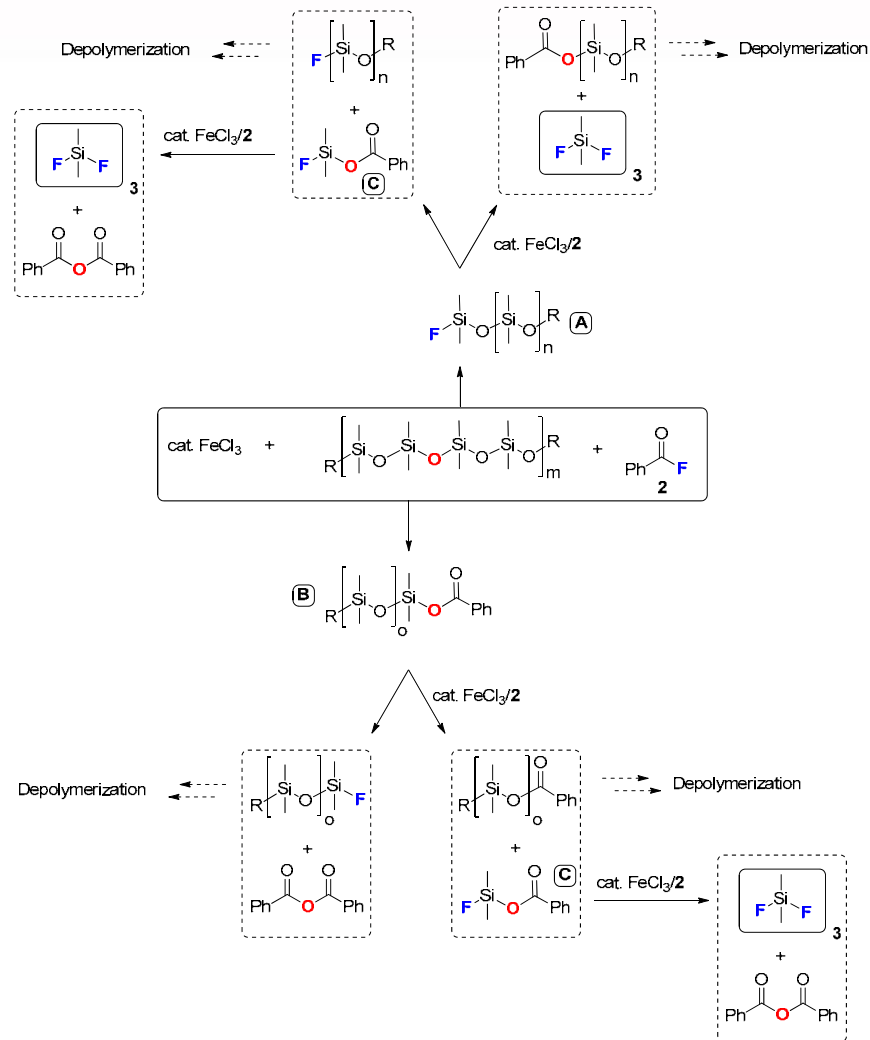


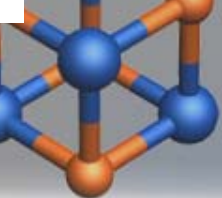
Reaction set-up



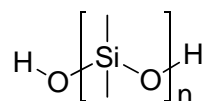
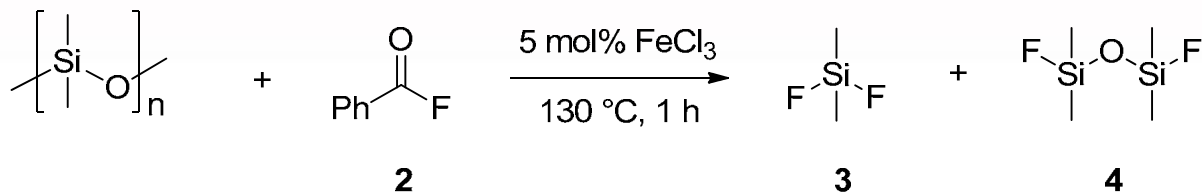


Depolymerization of Silicones

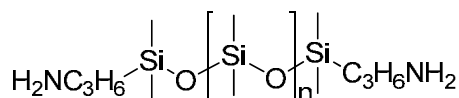




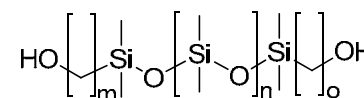
Depolymerization of Silicones



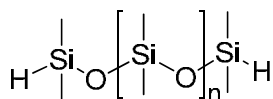
88% yield (69/19)
($M_n \sim 110.000$ g/mol)



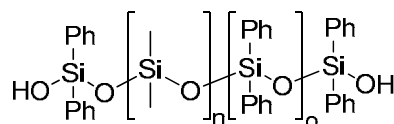
56% yield (47/9)
($M_n \sim 2.500$ g/mol)



95% yield (72/23)
($M_n \sim 5.600$ g/mol)



65% yield (49/16)
($M_n \sim 580$ g/mol)

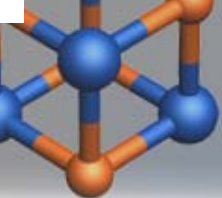


60% yield (40/10)^{a)}
($M_n \sim 580$ g/mol)
87% yield (Ph_2SiF_2)

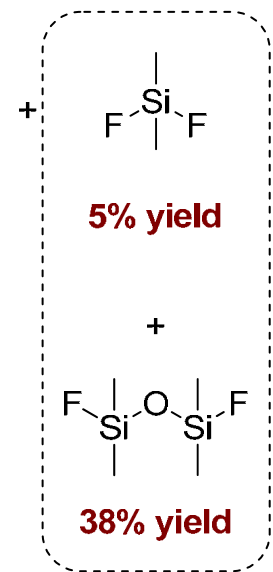
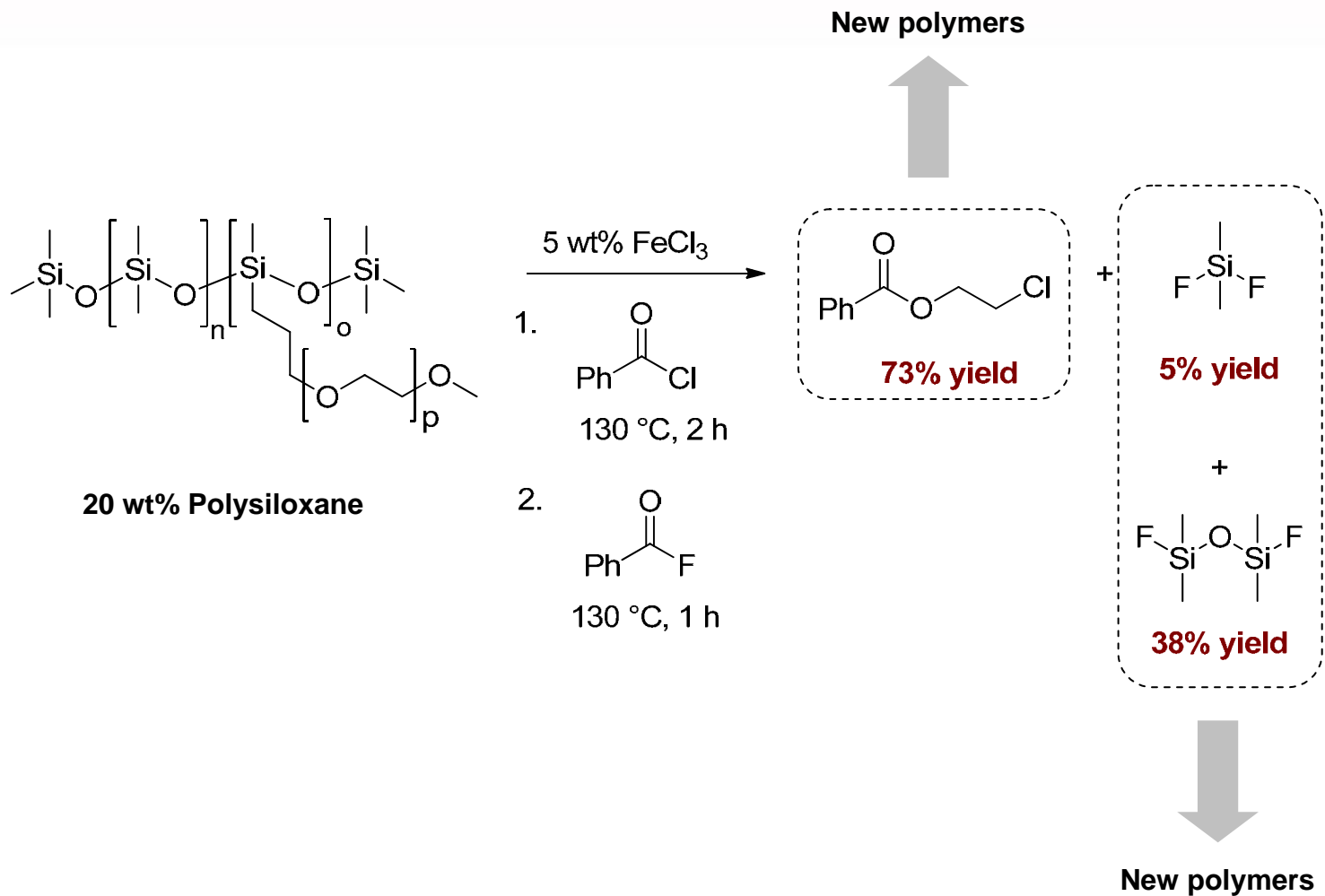
Silicone oil
(viscosity 30.000 cSt)

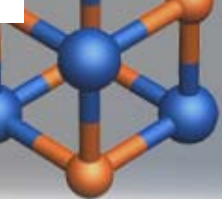
81% yield (74/7)

a) 95:5 mole ratio of dimethylsiloxane:diphenylsiloxane

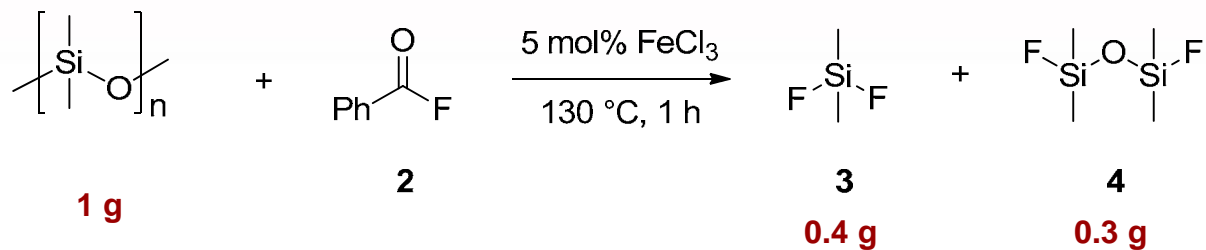


Depolymerization of Silicones

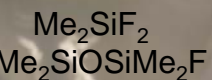


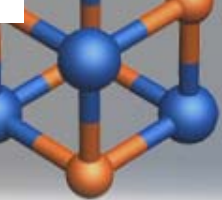


Depolymerization of Silicones

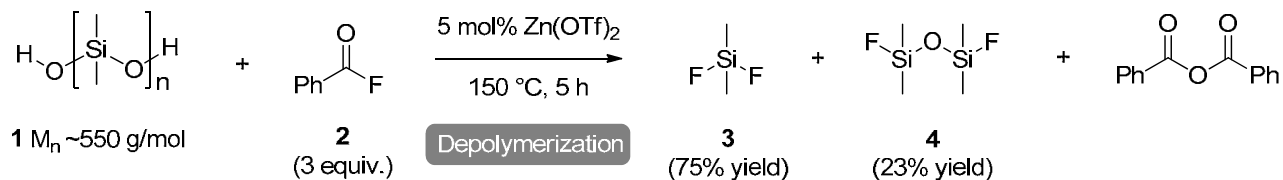
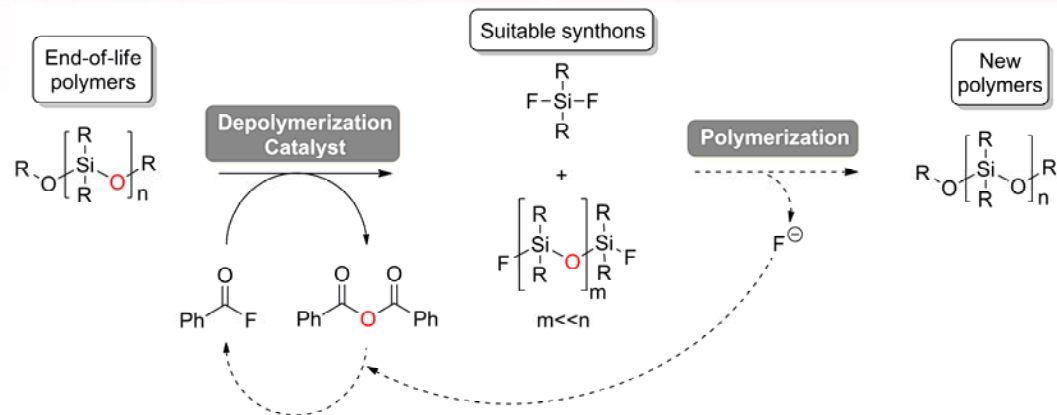


Silicone baking cup

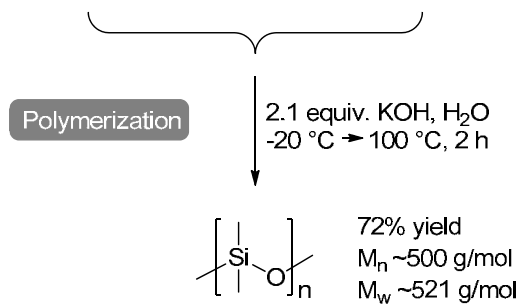


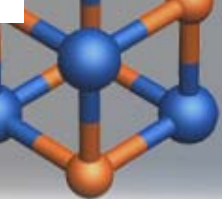


Depolymerization of Silicones

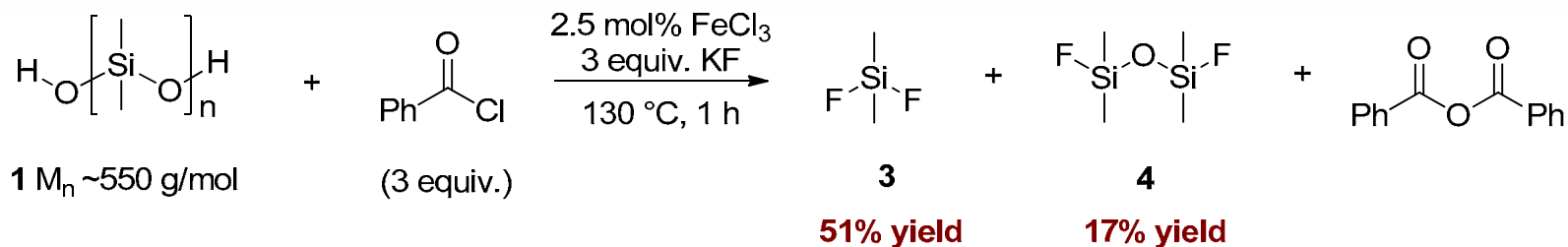


PhC(O)F: ~482 €/mol

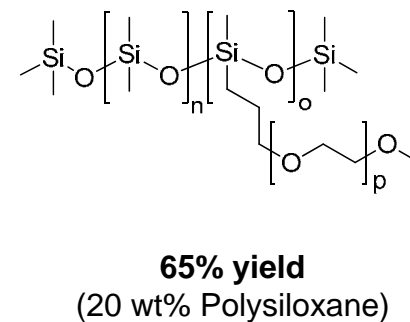
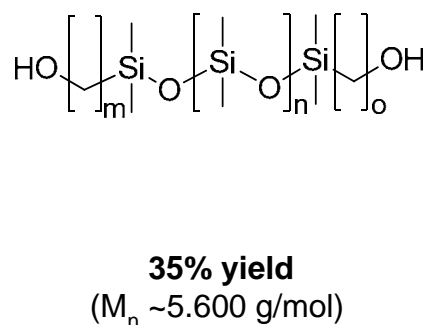
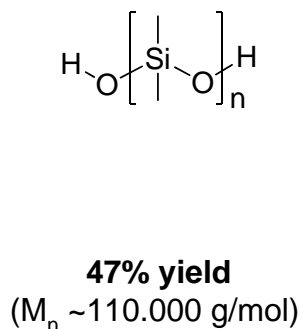


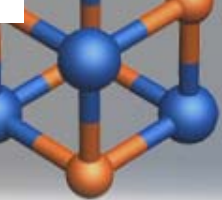


Depolymerization of Silicones

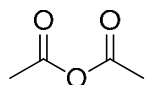
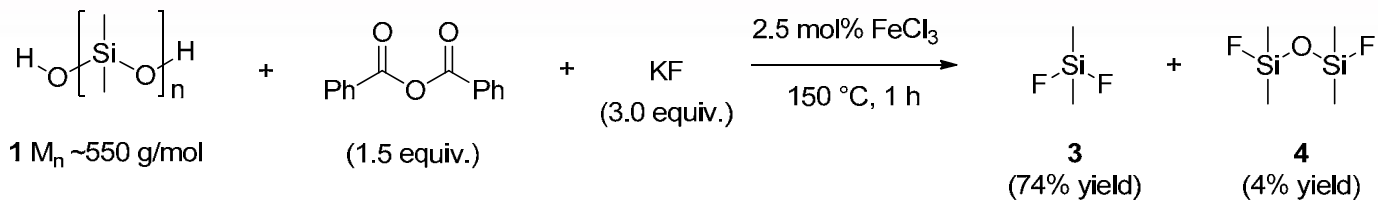


PhC(O)Cl/KF: ~22 €/mol
PhC(O)F: ~482 €/mol

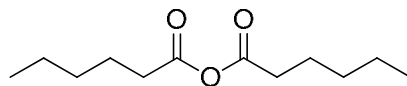




Depolymerization of Silicones

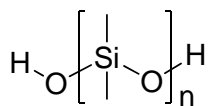


3: 36% yield
4: 4% yield

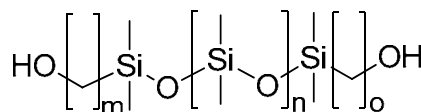


3: 78% yield
4: 1% yield

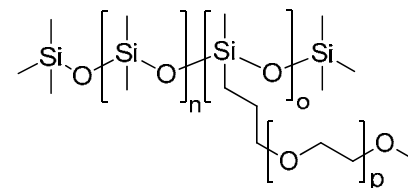
PhC(O)O(O)CPh/KF: ~46 €/mol
PhC(O)Cl/KF: ~22 €/mol
PhC(O)F: ~482 €/mol



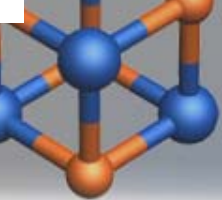
60% yield
 ($M_n \sim 110.000$ g/mol)



48% yield
 ($M_n \sim 5.600$ g/mol)

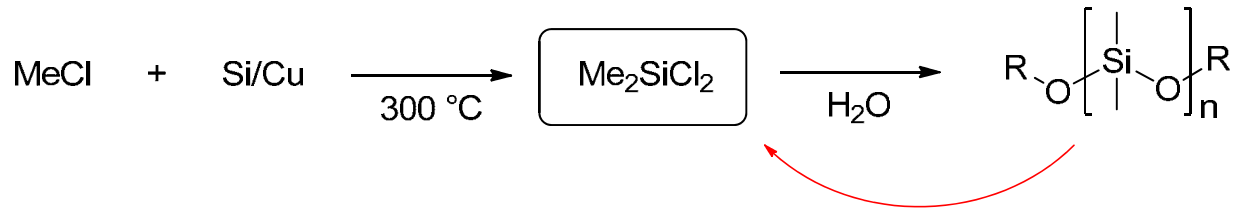


71% yield
 (20 wt% Polysiloxane)

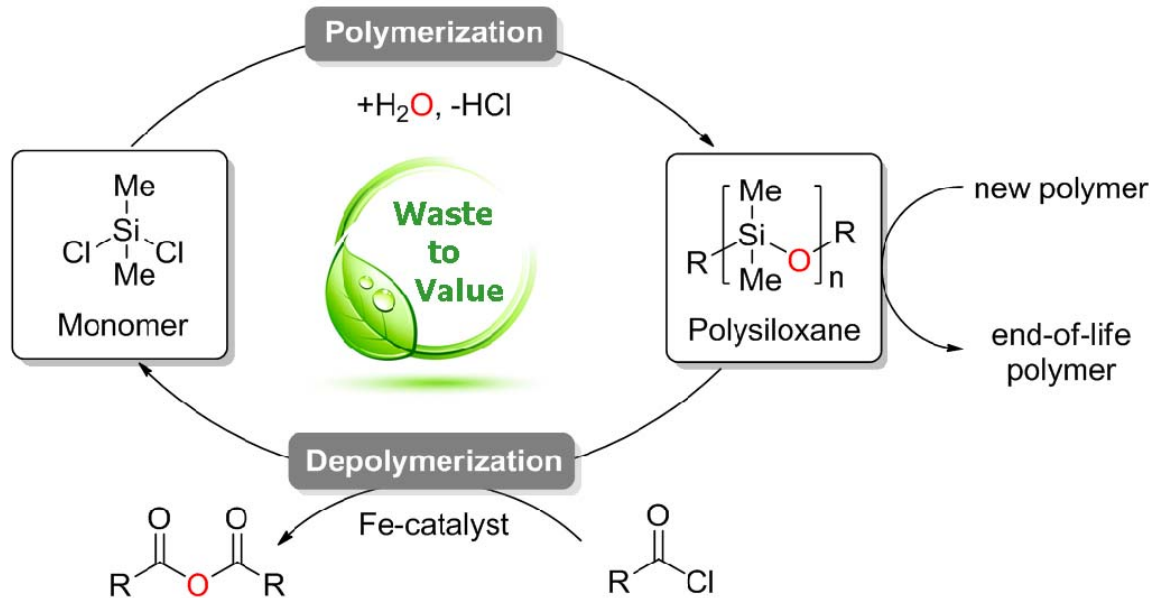


Depolymerization of Silicones

■ Silicone Synthesis:

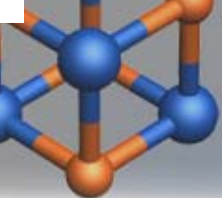


■ Silicone Recycling:

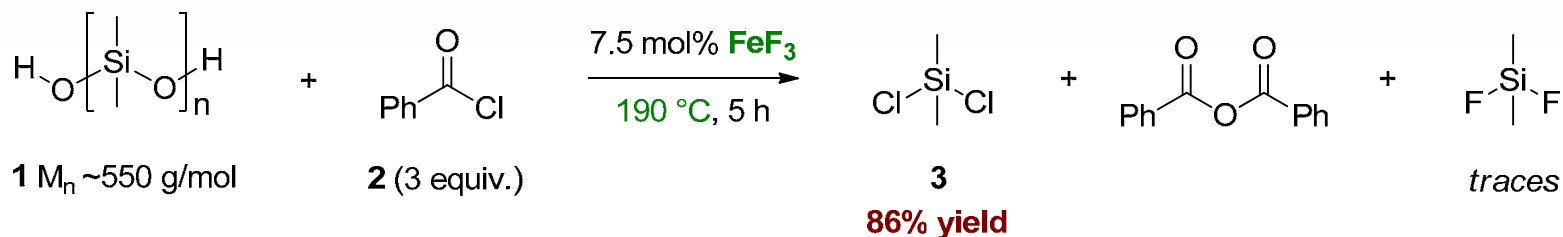


■ B. A. Ashby, GB 990657, **1965**.

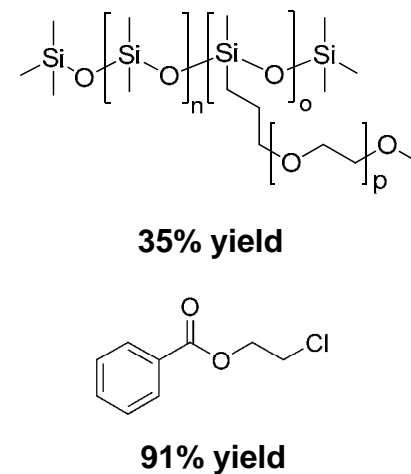
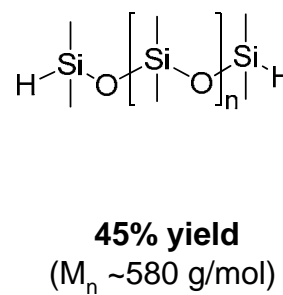
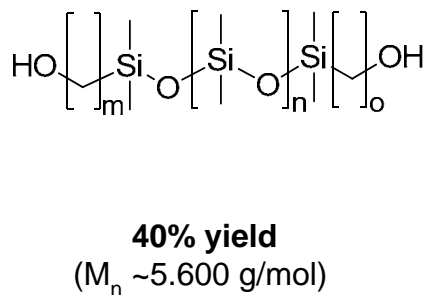
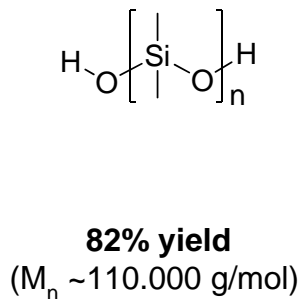
■ S. N. Borisov, M. G. Voronkov, N. G. Sviridova, *Zh. Obshch. Khim.* **1969**, 39, 559-564.

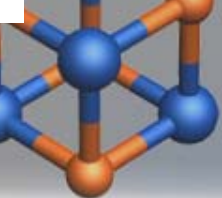


Depolymerization of Silicones



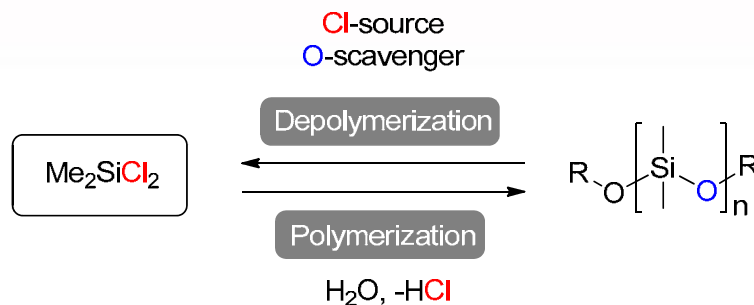
(FeCl₃: 32% yield)





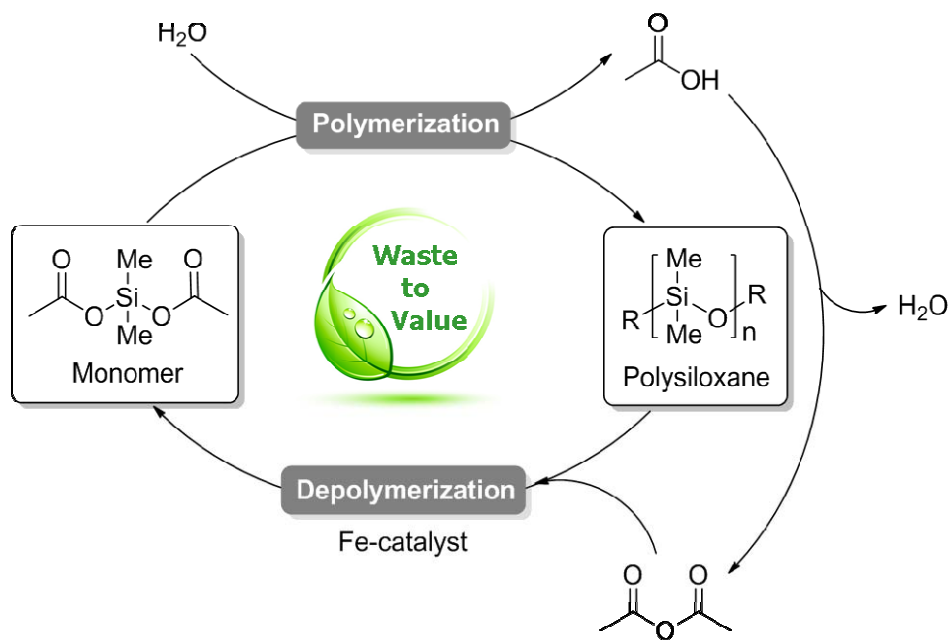
Depolymerization of Silicones

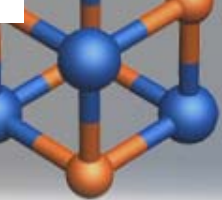
■ Polymerization/Depolymerization:



■ Silicone Recycling / Depolymerization Reagent Recycling:

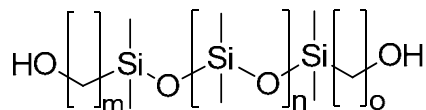
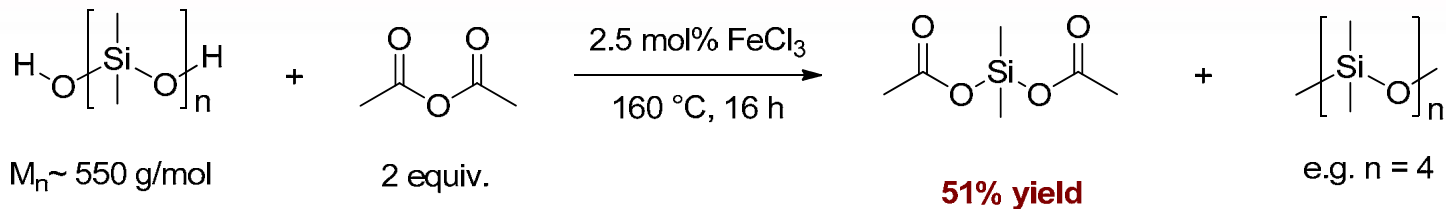
Ac₂O: ~3 €/mol
 PhC(O)Cl/KF: ~22 €/mol
 PhC(O)O(O)CPh/KF: ~46 €/mol
 PhC(O)F: ~482 €/mol



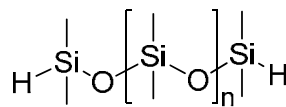


Depolymerization of Silicones

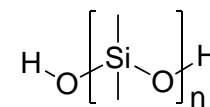
Depolymerization:



37% yield
($M_n \sim 5.600 \text{ g/mol}$)

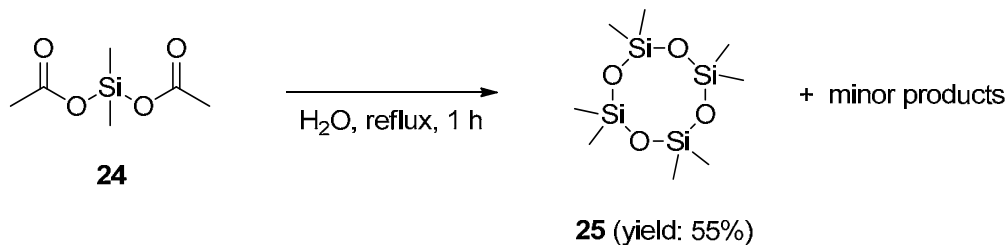


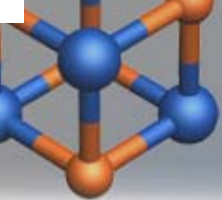
35% yield
($M_n \sim 580 \text{ g/mol}$)



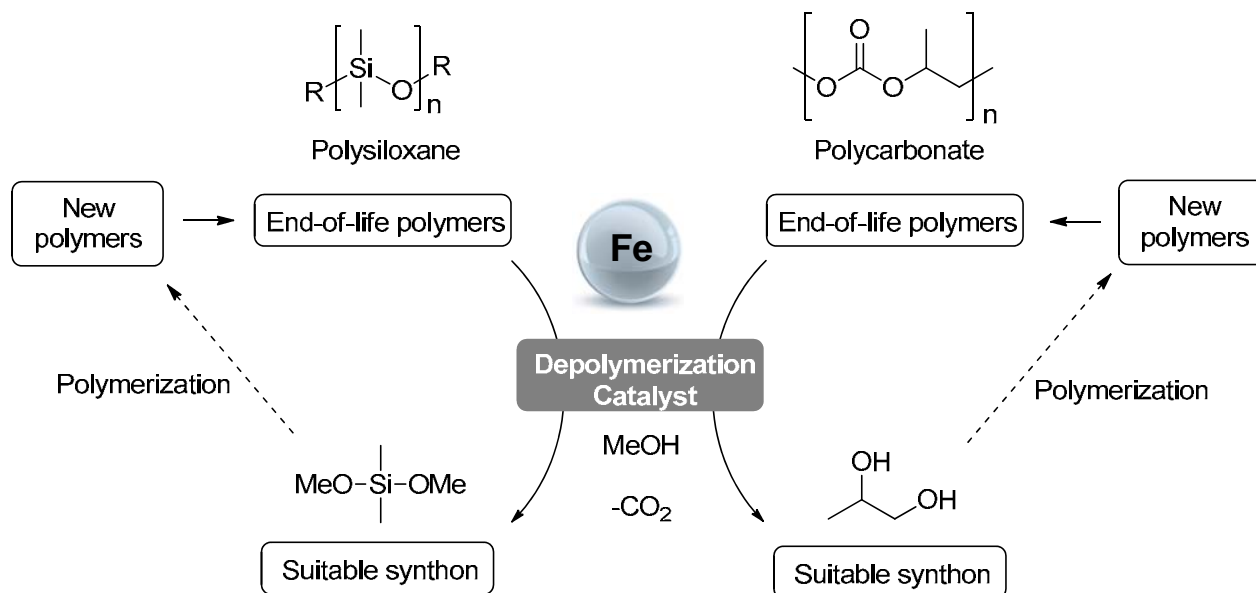
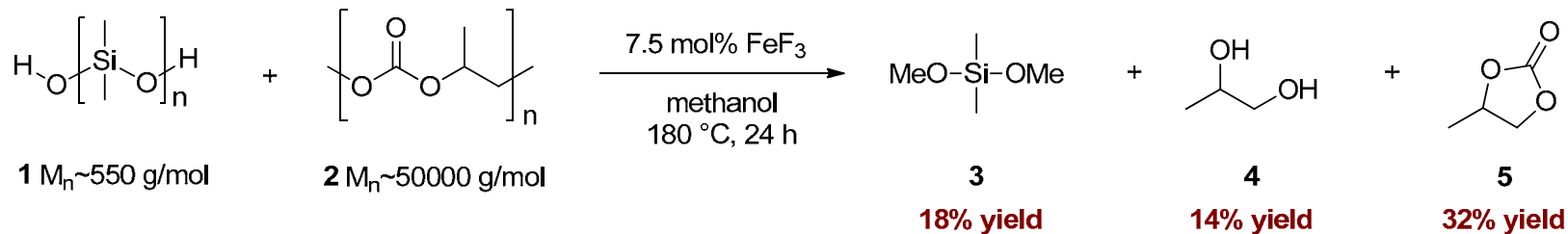
29% yield
($M_n \sim 110.000 \text{ g/mol}$)
 $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$

Polymerization:

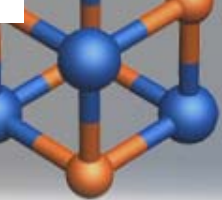




Depolymerization of Silicones

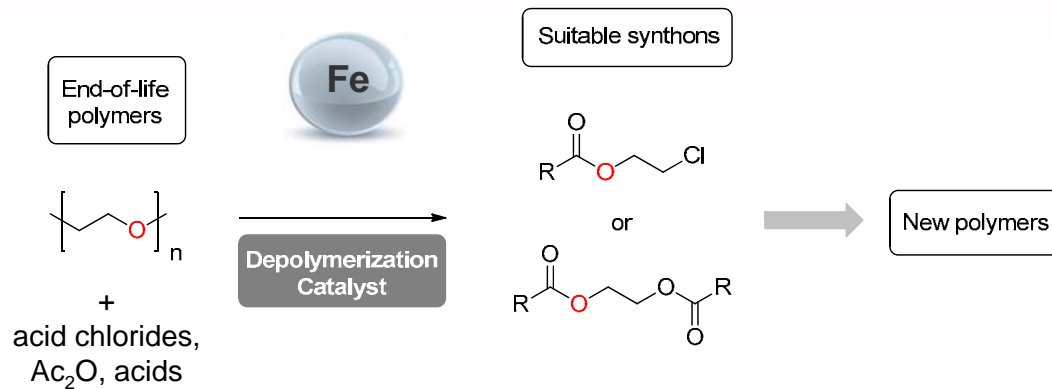


- a) M. Okamoto, S. Suzuki, E. Suzuki, *Appl. Catal. A: General* **2004**, 261, 239-245
- b) M. Okamoto, K. Miyazaki, A. Kado, S. Suzuki, E. Suzuki, *Catal. Lett.* **2003**, 88, 115-118

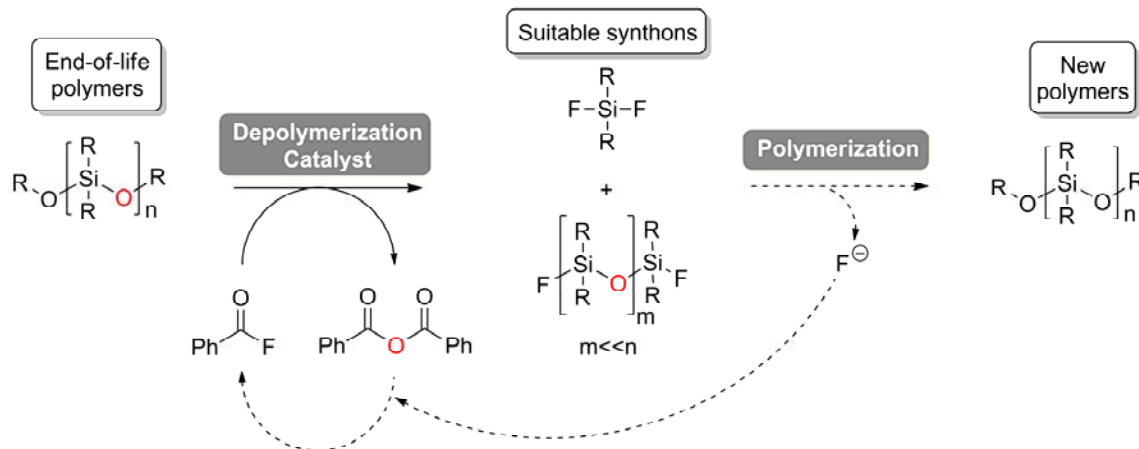


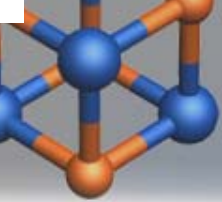
Summary

Depolymerization of Polyethers



Depolymerization of Polysiloxanes



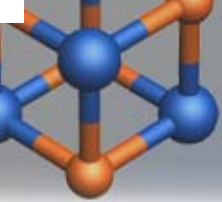


Acknowledgments



- Dr. Chika Inoue Someya
 - Dr. Michael Haberberger
 - Maik Weidauer
 - Peter Döhlert
 - Frank Czerny
 - Heidi Trutwin
-
- Prof. Shigeyoshi Inoue (TUB)
 - Dr. Elisabeth Irran (TUB)
 - Dr. Jan Dirk Epping (TUB)
 - Dr. Robert Kretschmer
(University of California San Diego)





Waste a “renewable“ resource for the future?



Thank you for your attention!